AMENDMENTS TO THE CLAIMS:

This listing of claims will replace all prior versions, and listings, of claims in the application:

LISTING OF CLAIMS:

- 1. (Original) A process for the conversion of syngas using a Fischer-Tropsch reactor, the process comprising:
 - a) forming a first syngas;
 - b) reacting at least a portion of the first syngas containing at least about 2 vol% CO₂ in a Fischer-Tropsch reactor to form a first hydrocarbonaceous product and a second syngas comprising at least about 2 vol% CO₂;
 - c) mixing the second syngas with a hydrogen-containing stream to provide an adjusted syngas having a molar ratio of H₂:(CO+CO₂) of at least about 1.0; and
 - d) reacting at least a portion of the adjusted syngas in a dual functional syngas conversion reactor to form a second hydrocarbonaceous product and a third syngas comprising a reduced amount of CO₂ than was present in the adjusted syngas.
- 2. (Original) The process of claim 1, wherein at least a portion of the third syngas is used as a fuel in the process.
- 3. (Original) The process of claim 1, wherein the Fischer-Tropsch reactor is a reactor selected from the group consisting of a slurry bed reactor, a fixed bed reactor, a fluidized bed reactor and combinations thereof.
- 4. (Original) The process of claim 1, wherein the Fischer-Tropsch reactor is a slurry bed reactor comprising a Fischer-Tropsch catalyst that comprises cobalt.
- 5. (Currently Amended) The process of claim 1, wherein the dual functional syngas conversion reactor comprises a catalyst comprising at least one element selected

from the group consisting of copper, chromium, alumina, zinc, iron, cobalt, nickel, ruthenium, thorium, rhodium, osmium and combinations thereof.

- 6. (Original) The process of claim 5, wherein the catalyst comprises a zeolite.
- 7. (Original) The process of claim 6, wherein the zeolite has an MFI structure.
- 8. (Original) The process of claim 1, wherein the adjusted syngas has a molar ratio of H₂:(CO+CO₂) between about 1.25 and about 3.0.
- 9. (Original) The process of claim 1, wherein the dual functional syngas conversion reactor is operated under conditions including a temperature between about 300°C and about 500°C and a pressure between about 25 atmospheres and about 100 atmospheres.
- 10. (Original) The process of claim 9, wherein the temperature is between about 375°C and about 425°C and the pressure is between about 35 atmospheres and about 75 atmospheres.
- 11. (Original) The process of claim 1, wherein CO₂ conversion in the dual functional syngas conversion reactor is between about 20% and about 80%.
- 12. (Original) The process of claim 1, wherein the hydrogen-containing stream mixed with the second syngas is obtained from a source selected from the group consisting of C₆-C₁₀ naphtha reformation, unreacted hydrogen from hydroprocessing a C₁₀₊-containing feedstock, syngas and combinations thereof.
- 13. (Original) The process of claim 1, further comprising recovering hydrogen for use in the hydrogen-containing stream by using a recovery process selected from the group consisting of adsorption, absorption, cryogenic separation, membrane separation and combinations thereof.

- 14. (Original) The process of claim 1, wherein the hydrogen-containing stream mixes with the second syngas at least one of before, during or after entering the dual functional syngas reactor.
- 15. (Original) A process for the conversion of syngas using a Fischer-Tropsch reactor, the process comprising:
 - a) forming a first syngas;
 - b) reacting at least a portion of a blended syngas, comprising at least a portion of the first syngas and containing at least about 2 vol% CO₂, in a Fischer-Tropsch reactor to form a first hydrocarbonaceous product and a second syngas comprising at least about 2 vol% CO₂;
 - c) mixing the second syngas with a hydrogen-containing stream to provide an adjusted syngas having a molar ratio of H_{2} :(CO+ CO₂) of at least about 1.0;
 - d) reacting at least a portion of the adjusted syngas in a dual functional syngas conversion reactor to form a second hydrocarbonaceous product and a third syngas comprising a reduced amount of CO₂ than was present in the adjusted syngas; and
 - e) blending at least a portion of the third syngas with at least a portion of the first syngas to form the blended syngas.
- 16. (Original) The process of claim 15, wherein the blended syngas has a CO₂ content of about 15 vol% or less.
- 17. (Original) The process of claim 16, wherein the CO₂ content is about 10 vol% or less.
- 18-20. (Canceled)